

Trans critical R744 for Food Industry

Freezing units -40° C



$\Box \quad THE \ PROJECT$

- □ REFRIGERATION EQUIPMENT
- □ HEAT RECOVERY
- □ MAIN INFORMATION
- PIPING AND PICTURES
- **COMPARISONS**
- □ CONCLUSIONS

<u>Preliminary remark</u>; The aim is not to oppose naturals refrigerants (NH3 et CO2), but TO SHOW THAT CO2 TC IS A POTENTIAL ALTERNATIVE, taking into account investment, running costs, safety, maintenance team skills, local regulations ...

SUMMARY



□ 1 Low temperature cold room for raw (and final products) at -25° C

- □ Some positive cold room to elaborate product at + 8° to +10° C
- □ 1 cooking line needing 1.5 ton/hour of vapor
- □ 2 Spiral freezers for "meat pallets" called « Bouchons » (Based on Chicken or Pork Meat with Reunion Island typical spices (combava) wrapped in rice leaf)

THE PROJECT

- □ 2 Medium temperature platforms with multi head weighers at -2° C
- **\Box** 1 conditioning room at + 12 ° C
 - 1 Low temperature "buffer" cold room for day production at -20° C
- □ 1 loop for 2.6 m3/h sanitary water



First CO2 TC unit

- **Booster TC unit with pumped CO2**
 - Refrigeration for 2 Spiral freezers (1 700 kg/h unit.)
- □ Heat recovery
 - For Sanitary water and water boiler heating up

Second CO2 TC unit

Booster TC unit with Direct expansion CO2

- For Glycol cooling to ice storage accumulator system
- For DX to L.T. cold room air coolers

DAY and NIGHT running conditions

- DAY : CO2 DX Refrigeration of 'Buffer" L.T. cold room
- NIGHT : CO2 DX Refrigeration of L.T. main cold room and Glycol cooling to Ice production in accumulator

ICE accumulator

Chilled water +1/+3° C for positive cold rooms

Refrigeration Equipment



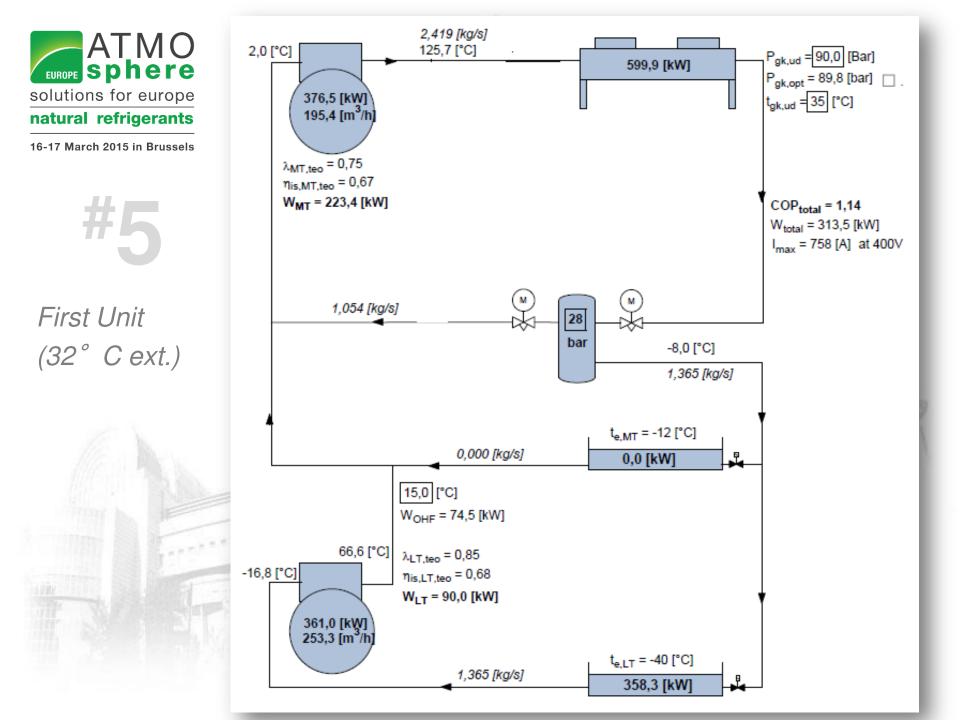
- <u>First unit booster</u>CO2 TC
 - MT level
 - Intermediate load
 - LT level
 - Low Temp load

-12°C 0 kW - 40°C 358 kW

First Unit

- 8 semi hermetic Bitzer compressors on M.T. (1 with inverter)
- 5 semi hermetic Bitzer compressors on L.T. (1 with inverter)
- 1 low pressure vessel
- 2 R744 refrigerant pump with variable flow
- 1 heat recovery plate exchanger
- 1 desuperheater
- 1 H.C. resilient cooler
- 1 gaz cooler
- CO2 charge : 1300 kg







Second unit booster CO2 TC

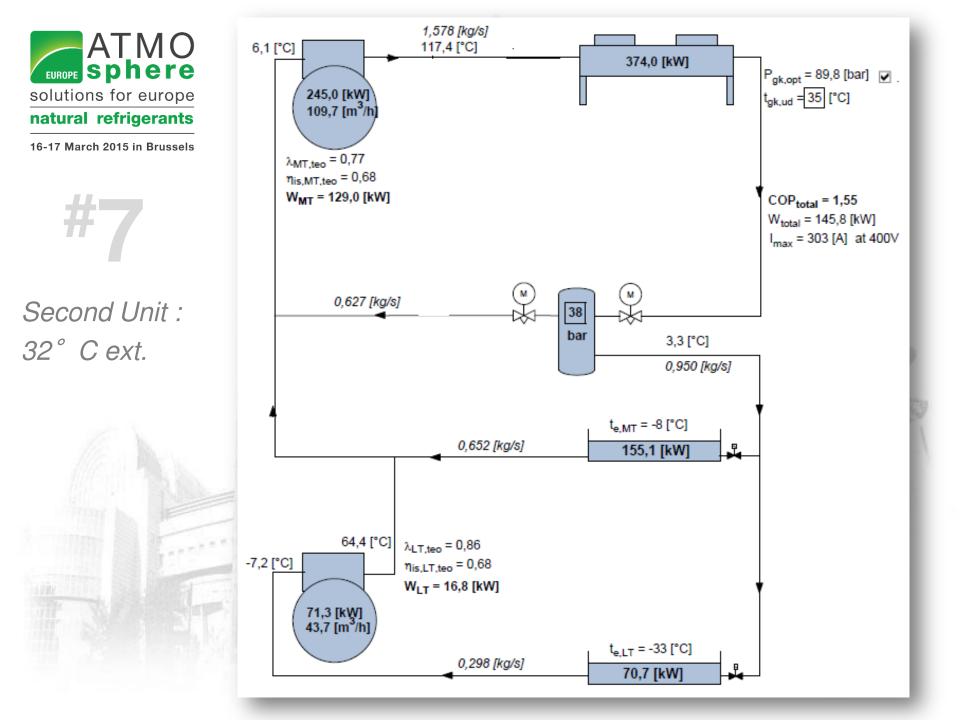
- Mode
- MT level
- Intermediate load
- LT level
- Low Temp load

Second Unit

with Day/Nig	<u>ht mode</u>
DAY	NIGHT
-12° C	- 8° C (-2/-6 Glycol)
0 kW *	155 kW
- 29 ° C	- 33 ° C
20 kW	70 kW

* Can assist ice bank in case of more load requested

- **5** semi hermetic Bitzer compressors on M.T. (1 with inverter)
- 3 semi hermetic Bitzer compressors on L.T. (1 with inverter)
- 1 liquid line to M.T. expansion valve on glycol plate exchanger
- 1 liquid line to L.T. expansion valve on air coolers (Cold rooms and platforms)
- 1 desuperheater
- 1 gaz cooler
- CO2 charge : 250 kg





HEAT RECOVERY SYSTEM

- **1** 100% pre heating of water from +17 to +85° C for the vapor boiler.
- □ 100% of sanitary water heating: 2.6 m3/h to ° 65° C
- Water heating for vapor production is done on line as vapor (cooking) is needed continuously and at the same time as freezing
- heated sanitary water is accumulated on storage tank; the water is used partly for product but mainly for cleaning all conveyors and process machines

SET of INSTRUMENTATION, MESURING and PROCESS CONTROLS

- ❑ Programmers for each room for day/night operation
- Counter of energy recovered from ice accumulator
- Electricity measurements on main consumers
- (main supply line, racks, production, distribution ...)
- Gas and water consumptions
- Remote and monitoring control system
- Energy management



Heat Recovery and Controls



OWNER/INVESTOR :PLANT :

Main information

ASIA FOOD Reunion Island France : Le Mans (72)

AF Consulting

CONSULTANT REFRIGERATION :

CONTRACTOR :

AXIMA REFRIGERATION GDF SUEZ

SPECIFIC SUPPLIERS :

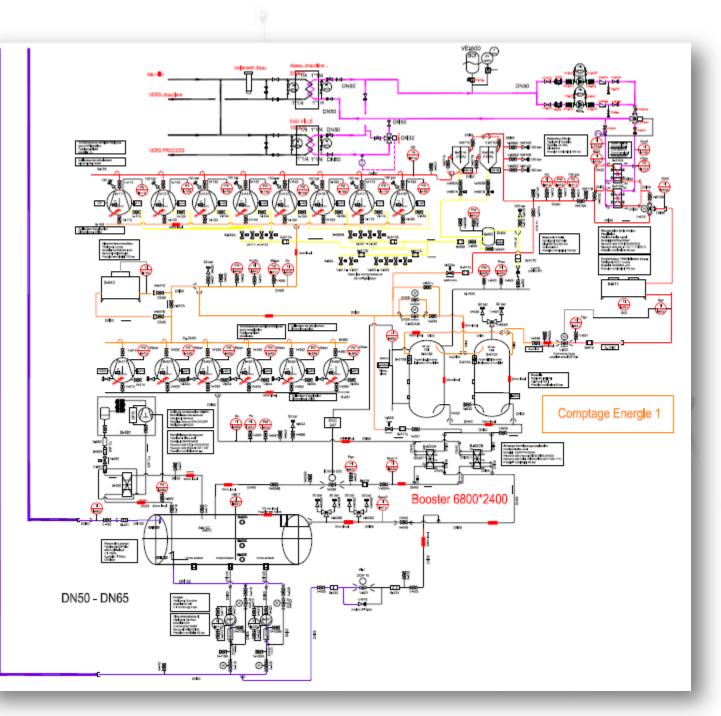
ADVANSOR (DK)for CO2FAFCO (CH)for ice aBITZER (D) for TC compressorsDANFOSS (DK)for TC unSINOFREEZE (CH)for SpiraCAREL (IT)for ColdALFA LAVAL (S)for CO2LUVATA (IT)for Gas ofCONTARDO (IT)for air con

for CO2 TC units for ice accumulator mpressors for TC units control for Spiral freezers for Cold room control for CO2 plate exchangers for Gas coolers for air coolers



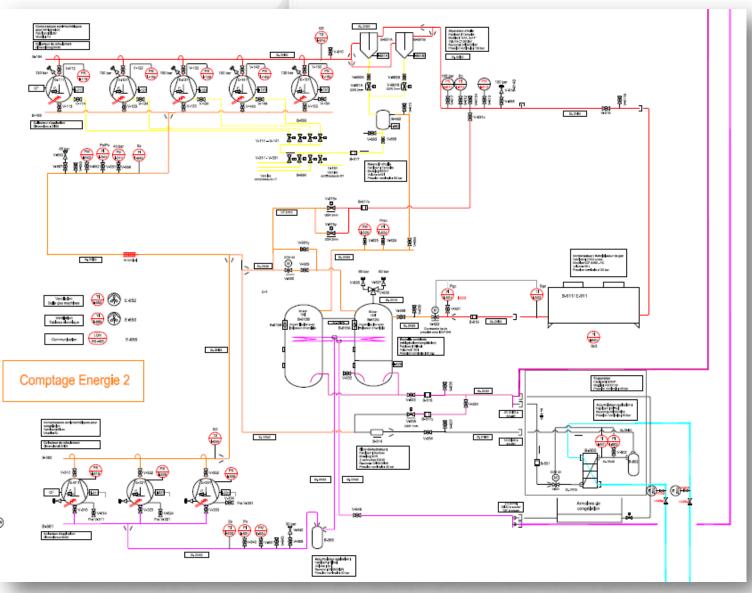
#-

R744 TC Pumped Booster Rack





R744 TC DX Booster Rack

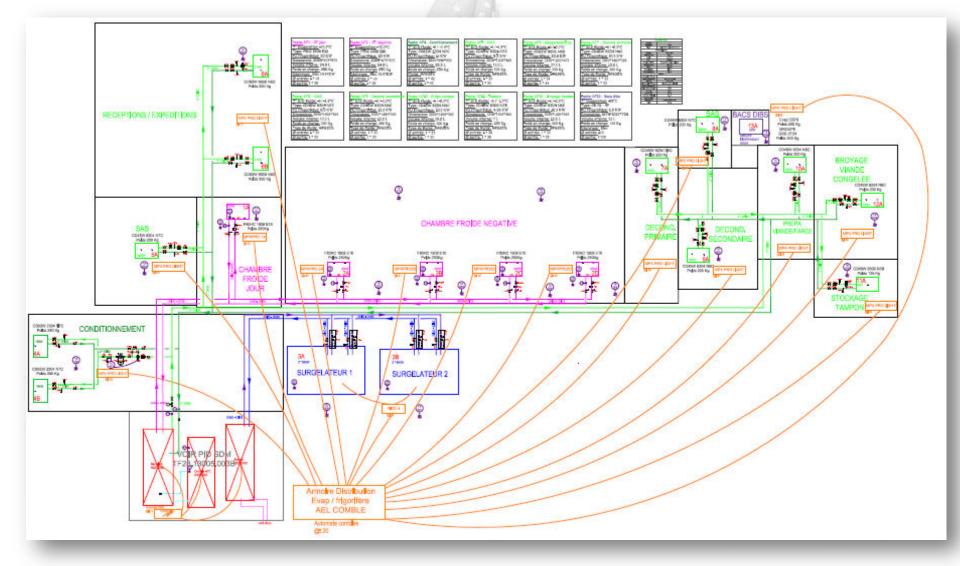




#12

Main diagram

16-17 March 2015 in Brussels





#13

The product : "Bouchons" in the Multi heads Weigher



The factory built end of 2013





The platform is cooling by DX CO2 from LT suction line of the Rack at -2° C





LT Vessel and inverter pumps side

The pumped R744 Rack



Compressors and Liquid receivers side







:15



Piping- Ice Storage – Gas cooler – Rack TC









The overall Machines room

#16



Loft piping CO2 & Chilled water







Freezer regulation equipment





Refrigeration users



Chilled water cold room





Cold Room regulation equipment





Solutions Comparison

H.F.C. SOLUTION ?

- Witch refrigerant for low temperature and pumped circulation ?
 - R404A/R507 ? -> G.W.P. !!
 - High refrigerant cost
 - Carbon tax ? Not yet in France but ...
 - Leak Rate !
 - Short sustainability

AMMONIA SOLUTION ?

- Refrigerant charge above 1 500 kg introduce declaration process in France
 - Plant less than 10 meters from neighbor !
 - Safety for working peoples and products during storage and production
 - Equipment's for safety, detection, alarms ...
 - Qualify the plant every 5 years
 - **Costs of NH3 distribution piping (see following tables)**
 - Costs of water for condensation (make up, treatment, controls)

CASCADE (HYBRID) SOLUTION CO2/NH3 ?

- Less NH3 and No ammonia in rooms
- But still ammonia outside. Either evaporative (Water !) either air condenser (less performance and higher risk)

CASCADE (HYBRID) SOLUTION CO2/H.F.C. ?

- One solution when Ammonia is problem face to regulation and/or price
- Flooded reliable system with high amount of R134a then Problems of H.F.C ...



Solutions Comparison

SOLUTION CO2 TC

- Good COP considering local ambient conditions, nights running time, accumulation facility
 - Lower cost for distribution piping
 - No need of water for condensation
 - Important potential of heat recovery until 100% of discharged HP heat
 - Evaporators compacts, lights, performants and quick to defrost
 - Plant servicing open to more suppliers
 - Less stress for plant handling
 - More simple refrigerant management
 - More product and personal safety
 - Good compromise investment/running costs !



Solutions Comparison

	R404 A	NH3	NH3/CO2 cascade	R134a/CO2 flood cascade	TC Booster CO2
			Industrial & commercial	Industrial & commercial	
Informations	commercial compressors	Industrial compressors	compressor	compressor	Commercial compressor
	Pumped and DX	Pumped + Glycol	Pumped CO2 + Glycol	Pumped CO2 + Glycol	Pumped and DX
	Air condenser	Evaporative condenser	Air condenser	Air condenser	Air condenser
French and European regulation	Very restrictive	Restrictive	Not so restrictive	Not so restrictive	No restrictive
	YES F-Gas	YES NH3 > 1500 kg (FR)	YES NH3 > 150 kg	YES F-Gas	
	HIGH GWP	YES evaporative system (FR)	No evaporative system	GWP > 150 but cascade R134a	
		YES HP liquid outside (FR)		No evaporative system	
Sustainability	Very Short	Good	Good	Short	Good
Maintenance costs	Very High	High	Medium	Medium	Low
	Leak integrity	Mechanic maintenance	Mechanic maintenance	Mechanic maintenance	Medium skill
	Refrigerant cost	Water treatment	High skill	Refrigerant cost	
	Leak Rate/High amount	Water consumption		Leak Rate/High amount	
	Carbon tax ?	High skill		Carbon tax ?	
				High skill	
Water consumption	NO	YES	NO	NO	NO
Running costs (Maintenance, energy, heat recovery)	150 %	130 %	120 %	110%	100%
Investment	100 %	140 %	160 %	120 %	108 %
Refrigeration effciency	117 %	100 %	107 %	110 %	105 %
Heat recovery potential	Limited	Medium	Medium	Limited	Good
T.E.W.I.	+ 2 800%	1	+ 7%	+ 670 %	+ 5%



Solutions Comparison : Piping

Base 250 kW	Vapor -10°C			Vapor -40°C		
	CO2	NH3	R507	CO2	NH3	R507
Vaporization heat kJ/kg	258.6	1297	170	435.3	1389	191.5
Specific volume of vapor m3/kg	0.014	0.42	0.043	0.038	1.55	0.13
Mass flow kg/s	0.967	0.193	1.47	0.574	0.18	1.305
Vapor volume flow m3/s	0.014	0.081	0.063	0.022	0.28	0.17
Ratio of vapor volume flow	1	5,8	4,5	1	12,7	7.7



Conclusion

The CO2 TC SOLUTION WITH PUMP CIRCULATION IS OF COURSE A MUCH BETTER SOLUTION THAN ANY H.F.C. ALTERNATIVE BUT ALSO AN INTERESTING ALTERNATIVE TO USUAL AMMONIA SOLUTION

As soon as:

- Evaporating temperature is low between -35 to 54°C
- Distribution piping is important
- Heat needed at high temperature level
- Maintenance team is not so skilled
 - Local regulation and constraints for ammonia are important
 - Weather condition are suitable for average good efficiency

WAYS OF IMPROVEMENT

- Compress separately the « flash gas » witch can represent 40% of the mass flow M.T. Study some solution on DX similar to flooded solution with ejector
- Find sub cooling sources
- Follow the evolution of compressor to bigger ones

EUROPE ATANO Solutions for europe natural refrigerants

16-17 March 2015 in Brussels

THANKS FOR YOUR ATTENTION

Mr Vincent RIVET afconsulting@sfr.fr +33 (0)6 62 47 07 01